To:

#### From the INTERNATIONAL BUREAU

## **PCT**

## **NOTIFICATION OF ELECTION**

(PCT Rule 61.2)

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Date of mailing (day/month/year)
29 June 2000 (29.06.00)

In its capacity as elected Office

PCT/EP99/08901

Applicant's or agent's file reference
TS 0764 PCT

International filing date (day/month/year)

O5 November 1999 (05.11.99)

Priority date (day/month/year)

O6 November 1998 (06.11.98)

**Applicant** 

DIRKSE, Hendrik, Arien et al

1.	The designated Office is hereby notified of its election made:
	X in the demand filed with the International Preliminary Examining Authority on:
	17 May 2000 (17.05.00)
	in a notice effecting later election filed with the International Bureau on:
2.	The election X was
	was not
	made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland Authorized officer

C. Villet

Facsimile No.: (41-22) 740.14.35

Telephone No.: (41-22) 338.83.38

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## INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant'	s or ag	ent's file reference	<del></del>	See Notification of Transmittal of International
TS 0764	4 PCT		FOR FURTHER ACTION	Preliminary Examination Report (Form PCT/IPEA/416)
1		lication No.	International filing date (day/mont	h/year) Priority date (day/month/year)
PCT/EP99/08901 05/11/1999			05/11/1999	06/11/1998
Internation C10G11		ent Classification (IPC) or r	national classification and IPC	
Applicant				
SHELL	INTE	RNATIONALE RESEA	ARCH et al.	
			mination report has been prepare according to Article 36.	d by this International Preliminary Examining Authority
2. This	REPO	ORT consists of a total of	of 6 sheets, including this cover s	sheet.
1	been a	mended and are the ba	•	ne description, claims and/or drawings which have containing rectifications made before this Authority ions under the PCT).
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3. This	report	contains indications re	lating to the following items:	
1	$\boxtimes$	Basis of the report		
П		Priority		
111		Non-establishment of	opinion with regard to novelty, in	ventive step and industrial applicability
IV		Lack of unity of invent		,
V	$\boxtimes$		under Article 35(2) with regard to ions suporting such statement	novelty, inventive step or industrial applicability;
VI		Certain documents ci	ted	
VII	$\boxtimes$	Certain defects in the	international application	
VIII		Certain observations	on the international application	
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# INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/EP99/08901

<ol> <li>Basis of the po</li> </ol>
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	the		on under Article 14 are referred to in this report as "originally filed" and are not annexed to o not contain amendments (Rules 70.16 and 70.17).):
	1-8		as originally filed
	Cla	ims, No.:	
	1-8		as originally filed
	Dra	wings, sheets:	
	1/2	-2/2	as originally filed
2.			puage, all the elements marked above were available or furnished to this Authority in the international application was filed, unless otherwise indicated under this item.
	The	ese elements were a	available or furnished to this Authority in the following language: , which is:
		• •	translation furnished for the purposes of the international search (under Rule 23.1(b)).
		the language of pu	ublication of the international application (under Rule 48.3(b)).
		the language of a 55.2 and/or 55.3).	translation furnished for the purposes of international preliminary examination (under Rule
3.			leotide and/or amino acid sequence disclosed in the international application, the y examination was carried out on the basis of the sequence listing:
		contained in the in	ternational application in written form.
		filed together with	the international application in computer readable form.
		furnished subsequ	ently to this Authority in written form.
		furnished subsequ	ently to this Authority in computer readable form.
			t the subsequently furnished written sequence listing does not go beyond the disclosure in oplication as filed has been furnished.
		The statement that listing has been fu	t the information recorded in computer readable form is identical to the written sequence rnished.
١.	The	amendments have	resulted in the cancellation of:
		the description,	pages:
		the claims,	Nos.:

1. This report has been drawn on the basis of (substitute sheets which have been furnished to the receiving Office in

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# INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/EP99/08901

		the drawings,	sheets:							
5.		This report has been considered to go bey						been made	e, since they	have beer
		(Any replacement sh report.)	eet contail	ning such	amendmen	nts must be	e referred to	under item	າ 1 and anne	exed to this
6.	Add	litional observations, il	f necessar	y:						
٧.		soned statement un tions and explanatio					, inventive	step or ind	lustrial appl	licability;
1.	Stat	ement								
	Nov	relty (N)	Yes: No:	Claims Claims	1-8					
	Inve	entive step (IS)	Yes: No:	Claims Claims	1-8					
	Indu	ıstrial applicability (IA)	Yes: No:	Claims Claims	1-8					
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2. Citations and explanations see separate sheet

## VII. Certain defects in the international application

The following defects in the form or contents of the international application have been noted: see separate sheet

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## **EXAMINATION REPORT - SEPARATE SHEET**

## Re Item V

Reasoned statement under Rule 66.2(a)(ii) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

Claim 1 - Novelty

Claim 1 is a claim for a separator apparatus comprising a hollow circular housing connected to a dipleg, a gas outlet tube, an inlet means and a sieve.

The document D1: US-A-4 670 410 (BAILLIE LLOYD A) 2 June 1987 (1987-06-02) is regarded as being the closest prior art to the subject-matter of claim 1 and discloses (the references in parentheses applying to this document): an apparatus which accomplishes separation of solid catalyst particles from vapor (col 3, line 38-40) comprising an upright hollow circular housing (fig 2, ref 54 & col 4, line 2-3) connected to a dipleg (fig 1), a gas outlet (col 4, line 15) protruding co-axial from the top of the housing (fig 2), an inlet that is situated so that movement of the fluid stream mixture within the chamber causes solid particles to move in vortex fashion (col 4, line 50-51), and a plate (ref 121 & 134) having a plurality of holes (ref 124)(such a plate can be regarded as a sieve) positioned between the lower part of the circular housing and the upper part of the dipleg (fig 7 and 8). It is clear from fig 7 and 8 that the openings in the sieve are going to block particles exceeding 0.75 times the diameter of the dipleg, thus the sieve of D1 has openings which do not allow particles having a diameter greater than 0.75 times the diameter of the dipleg to pass the sieve and enter the dipleg.

The subject-matter of claim 1 therefore only differs from that known in the prior art D1 for the following reason: D1 does not disclose that the total area of openings in the sieve is greater than 2 times the cross sectional area of the dipleg. Thus the subjectmatter of claim 1 can be regarded as novel (Article 33 (2) PCT).

Claim 1 - Inventive Step

The problem to be solved by the present invention may therefore be regarded as preventing the dipleg from clogging.

The solution to this problem proposed by the present application can then be regarded

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as the provision of a sieve with a total area of openings greater than two times the cross sectional area of the dipleg.

The solution proposed in claim 1 of the present application cannot be considered as involving an inventive step (Article 33 (3) PCT) for the following reasons.

The problem to be solved seems to be already solved by the solution presented in D1 which also prevents clogging of the cyclone by means of a filter. The solution of the current application might still achieve a good separation efficiency but is actually just an alternative. In fact, the good separation efficiency has never been shown in the application. The necessary technical data has not been presented to show that the presented solution actually solves the problem or that an improvement over the prior art is obtained.

Claim 2 - 7 - Novelty - Inventive Step

Since claim 1 is novel, the dependent claims 2 - 7 also meet the requirements of Article 33 (2) PCT.

However, D1 further discloses a vortex stabilizer on top of the sieve (col 3, line 47-48 and fig 7 & 8) and an inlet means tangentially arranged at the upper part of the circular housing (fig 2 & 4).

Thus, the addition of these features to claim 1 would not render its subject-matter inventive.

#### Claim 8 - Novelty

Claim 8 is a claim for a fluid catalyst cracking process in which catalytic particles are separated from a gaseous reactor effluent in at least two sequential separation steps using an apparatus according to claims 1 -7.

The subject-matter of claim 8 is novel (Article 33 (2) PCT) over D1 for the same reasons as mentioned for claim 1.

Claim 8 - Inventive Step

D1 discloses a process for hydrocarbon cracking using solid catalyst particles where the catalytic particles are separated from an effluent (col 3, line 20-23) using two or

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## INTERNATIONAL PRELIMINARY

International application No. PCT/EP99/08901

**EXAMINATION REPORT - SEPARATE SHEET** 

more separators as described before (col 4, line 66-68 - col 5, line 1-2). Thus, for the same reasoning as put forth in claim 1, the subject-matter of claim 8 cannot be considered to involve an inventive step (Article 33 (3) PCT).

## Re Item VII

## Certain defects in the international application

To meet the requirements of Rule 5.1 a) ii) PCT, the document D1 should be identified in the description and the relevant background art disclosed therein should be briefly discussed.

The features of the claims are not provided with reference signs placed in parentheses (Rule 6.2(b) PCT).





## INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference TS 0764 PCT	FOR FURTHER ACTION	see Notification of (Form PCT/ISA/22	Transmittal of Inte	mational Sear e applicable, i	ch Report item 5 below.
International application No.	International filing date (da	tv/month/veer)	(Earliest) Priority	Data (day/mo	enth (rose)
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This international Search Report has been according to Article 18. A copy is being tra	n prepared by this internation unsmitted to the internationa	nal Searching Autho I Bureau.	ority and is transmit	ted to the app	Dicant
This international Search Report consists  It is also accompanied by	of a total of2 a copy of each prior art doc	sheets. ument cited in this r	eport.		
1. Basis of the report			· ·		· · · · · · · · · · · · · · · ·
<ul> <li>a. With regard to the language, the language in which it was filed, unk</li> </ul>	international search was car ess otherwise indicated und	ried out on the basi er this item.	s of the internations	al application i	n the
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international application as	s filed has been furnished.				
the statement that the info fumished	rmation recorded in comput	er readable form is i	dentical to the writt	en sequence l	listing has been
2. Certain claims were four	nd unsearchable (See Box	).			
3. Unity of invention is lack	úng (see Box II).				
4. With regard to the title,					
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the text has been establish	ned by this Authority to read	as follows:			
5. With regard to the abstract,					
the text is approved as subthe text has been establish within one month from the	omitted by the applicant. ned, according to Rule 38.2(I date of mailing of this intern	o), by this Authority ational search repo	as it appears in Bo t, submit comment	x III. The appl s to this Autho	icant may, ority.
6. The figure of the drawings to be public			2		•
as suggested by th applic	eant.			None of th	figures.
because the applicant falle	d to suggest a figure.				
because this figure better o	characterizes the invention.	_			



## **INTERNATIONAL SEARCH REPORT**



P* 771	ational	Application	Nc
	/EP	Application 99/089	01

A. CLASS	SIFICATION OF SUBJECT MATTER	/ == 05/ 00501
IPC 7	SIFICATION OF SUBJECT MATTER C10G11/18 B01J8/18 B04C5	5/14 B04C5/181
According	to international Patent Classification (IPC) or to both national cla	ssification and IPC
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C. DOCUM	ENTS CONSIDERED TO BE RELEVANT	
Category °	Citation of document, with indication, where appropriate, of the	
	or mere appropriate, or me	e relevant passages Relevant to claim No.
X	US 4 670 410 A (BAILLIE LLOYD / 2 June 1987 (1987-06-02) figures 2-8	1-8
Furths	er documents are listed in the continuation of box C.	
		Patent family members are listed in annex.
A" document consider to filing date.  L" document which is citation of document other me document later that	t which may throw doubts on priority claim(s) or ofted to establish the publication date of another or other special reason (as specified) at referring to an oral disclosure, use, exhibition or sens at published prior to the international filing date but in the priority date claimed	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention  "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.  "&" document member of the same patent family
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## INTERNATIONAL SEARCH REPORT

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Patent document cited in search report Publication date Patent family member(s) Publication date

US 4670410 A 02-06-1987 NONE

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## **PCT**





## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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Hague (NL).

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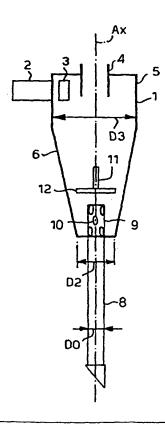
(75) Inventors/Applicants (for US only): DIRKSE, Hendrik, Arien [NL/NL]; Carel van Bylandtlaan 30, NL-2596 HR The Hague (NL). DRIES, Hubertus, Wilhelmus, Albertus [NL/NL]; Badhuisweg 3, NL-1031 CM Amsterdam (NL). STEIN, Louis, Edward [US/US]; 5818 Autumn Forest, Houston, TX 77092 (US). (81) Designated States: AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).

Published With international search report.

(54) Title: SEPARATOR APPARATUS

## (57) Abstract

A separator apparatus for separating solids from a gas-solid containing feed resulting in a gas-rich stream, the separator comprising: an upright hollow circular housing fluidly connected to a dipleg for discharging solids positioned below the housing; a gas outlet tube for discharging the gas-rich stream from the circular housing, which outlet tube protrudes substantially co-axial from the top of the housing; inlet means for the gas-solids feed so arranged to create, in use, a vortex flow in the circular housing; and a sieve positioned between the lower part of the circular housing and the upper part of the dipleg, which sieve has openings which do not allow particles having a diameter greater than 0.75 times the diameter of the dipleg to pass the sieve and enter the dipleg and wherein the total area of the openings in the sieve is greater than 2 times the cross-sectional area of the dipleg.



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#### SEPARATOR APPARATUS

## Background of the invention

The invention is directed to a separator apparatus for separating solids from a gas-solid containing feed resulting in a gas-rich stream, the separator comprising:

an upright hollow circular housing fluidly connected to a dipleg for discharging solids positioned below the housing;

a gas outlet tube for discharging the gas-rich stream from the circular housing, which outlet tube protrudes substantially co-axial from the top of the housing;

inlet means for the gas-solids feed so arranged to create, in use, a vortex flow in the circular housing.

Such an apparatus is described in US-A-5391289. This patent publication describes a cyclone separator which is used as a secondary separation step to separate solid catalyst particles from the reactor effluent of a fluid catalytic cracking (FCC) reactor. In a FCC process hydrocarbons are cracked at high temperature in the presence of a solid catalyst to more desired components, for example gasoline and lower olefins. In the field of FCC these cyclone separators are also referred to as secondary cyclones. Other publications describing these secondary cyclones in a FCC process are for example US-A-5055177, US-A-5376339, EP-A-299650, EP-A-488549 and EP-A-309244.

A disadvantage of these secondary cyclones is that coke deposit may form on the walls of these apparatuses. Coke forming is a result of the hydrocarbons present in the feed to the cyclone and the relatively high temperatures of the gasses fed to the cyclones. Large pieces of coke can fall from the wall into the dipleg and

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cause to clog the dipleg. When a dipleg is clogged the cyclone will not function in an optimal manner as a solid-gas separator and the fluid catalytic cracking process will have to be shut down in order to remove the coke from the dipleg. Because FCC processes are expected to run many months and even years between planned shutdowns any unexpected shutdown will cause considerable economic damage.

The object of this invention is to avoid the problems associated with clogging of the diplegs of the separator apparatus.

## Summary of the invention

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The object is achieved by the following apparatus. A separator apparatus for separating solids from a gas-solid containing feed resulting in a gas-rich stream, the separator comprising:

an upright hollow circular housing fluidly connected to a dipleg for discharging solids positioned below the housing; a gas outlet tube for discharging the gas-rich stream from the circular housing, which outlet tube protrudes substantially co-axial from the top of the housing, inlet means for the gas-solids feed so arranged to create, in use, a vortex flow in the circular housing; and a sieve positioned between the lower part of the circular housing and the upper part of the dipleg, which sieve has openings which do not allow particles having a diameter greater than 0.75 times the diameter of the dipleg to pass the sieve and enter the dipleg and wherein the total area of the openings in the sieve is greater than 2 times the cross sectional area of the dipleg.

It has been found that when such a sieve is used less problems due to clogging of the dipleg occur. Because of the sieve a reduction of the normal swirl movement in the dipleg is observed. As a result the pressure difference per length of dipleg will increase making it possible to

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use a shorter dipleg. This is very advantageous, especially when these cyclones are present within a vessel, for example a stripping vessel of a FCC process. The length of a dipleg is often the determining factor for the dimensions of the vessel. Thus shorter diplegs result in that smaller vessels can be employed.

## Brief description of the drawings

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The invention shall be further elucidated by means of the following figures. Figure 1 represent a vertical cross section of the separator apparatus according the invention. Figure 2 represents another embodiment of the invention, wherein the lower part of the housing is not present. Figure 3 represents a possible embodiment for a sieve combined with a vortex stabiliser. Figure 4 represents the upper part of a stripping vessel of a FCC process.

## Detailed description of the invention

Preferably the openings of the sieve do not allow particles greater than 0.5 times the diameter (D0) of the dipleg to pass the sieve.

Preferably the total area (A0) of the openings of the sieve is greater than 5 times the cross sectional area (A1) of the dipleg.

The circular housing of the separator may suitably have an upper tubular portion with a diameter (D3), a conical formed housing as a middle portion of which smaller diameter (D2) is at the lower end and optionally a lower part having a diameter (D1) which is greater than the diameter (D2) of the lower part of the conical housing. The diameter (D0) of the dipleg is suitably smaller than the diameter (D3) of the upper part of the circular housing of the separator. Preferably the volume of the circular housing at the level where the sieve is located is sufficiently large to allow coke particles to accumulate. The dimensions of the sieve will be so chosen

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that while coke particles accumulate in the lower part of the housing a sufficiently large number of openings are not blocked in order to allow the separated particles to enter the dipleg. The form of the holes is not very critical. Circular, rectangular holes and slots are possible forms for the openings in the sieve.

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The sieve is preferably positioned symmetrically around the axis just on top of the inlet opening of the dipleg. One embodiment of the invention is where the sieve is a tube placed on top of the dipleg which tube protrudes the circular housing from below. The tube has about the diameter of the dipleg and has an open lower end and a closed upper end. In the vertical walls of the tube holes are present.

The sieve is preferably sufficiently strong to avoid it being damaged by erosion due to the gas-solids moving in the circular housing. Protective linings can be applied to protect the upper part of the sieve. A more preferred method of protecting the sieve is by positioning a vortex stabiliser below the opening of the gas outlet tube and above the sieve. The vortex, present in use, will end at the top of the vortex stabiliser thereby reducing erosion of the sieve. The vortex stabiliser will additionally further reduce any swirl movement in the dipleg and thus increases the pressure difference per length of dipleg, which is advantageous for the reasons set out earlier.

The vortex stabiliser comprises suitably of a hat having a relatively large diameter and a vertically oriented vortex stabiliser rod placed on top of the hat having a considerably smaller dimension relative to the hat. The hat may be for example a circular plate or a cone. When a cone is used the top of the cone may function as a vortex stabiliser rod. Vortex stabilisers

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are also described in for example US-A-4692311, EP-A-360360 and EP-A-220768.

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A preferred embodiment is where the vortex stabiliser is placed on top of the sieve.

The vortex stabiliser may have a hollow tube as vortex stabiliser rod, wherein a fluid connection is present via the hollow tube between the top of the vortex stabiliser and a position below the vortex stabiliser and above the inlet of the dipleg.

The inlet means for the gas-solids feed can be axially or tangentially arranged at the upper tubular part of the circular housing.

The apparatus is preferably used as the second separation step (also referred to as secondary cyclone) to separate catalyst particles from a gaseous reactor effluent of a fluid catalyst cracking process in which the separation is conducted in at least two sequential separation steps.

A fluid catalytic cracking process comprises a reactor in which catalyst particles and gaseous hydrocarbons are contacted. The reactor is generally a vertically positioned tubular reactor often referred to as the riser reactor through which catalyst and reactants co-currently flow in an upwards direction. At the end of the riser the catalysts are separated from the reactor effluent. This separation is usually effected by means of one or more cyclones. The thus separated catalysts are collected in a stripping vessel. In this vessel the catalysts are stripped with a water containing gas to separate any hydrocarbons from the catalyst. The stripped catalysts are subsequently send to a regenerator vessel in which any coke is removed from the catalyst by means of combustion. The stripped and regenerated catalyst is reused in the process.

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The separation of catalyst from the reactor effluent is suitably performed by means of a first separator which separates the bulk of the catalyst, followed by a secondary cyclone which separates most of the remaining catalyst particles. Depending on the specific layout more than one secondary cyclone may be present operating parallel and/or in series of each other. These separator means may be placed inside the stripping vessel or outside the stripping vessel. Combinations of the two are also possible, wherein the primary separation means is placed inside the stripping vessel and the secondary cyclone is placed outside the stripping vessel. The advantages of the invention are especially apparent when the secondary cyclone is placed inside the stripping vessel because these cyclones cannot be easily inspected when the FCC process is in operation. Examples of such FCC configurations are described in the earlier cited patent publications US-A-5055177, US-A-5391289, EP-A-309244 and EP-A-299650. If the secondary cyclone is placed inside the stripping vessel the gas-solids feed inlet is preferably tangentially arranged.

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Preferably both the primary separation means, suitably a cyclone also referred to as the rough cut cyclone, and the secondary cyclone are placed inside the stripping vessel. More preferably the gas outlet of the rough cut cyclone is in fluid connection with the inlet of the secondary cyclone. This is advantageous because the residence time of the cracked hydrocarbons after they leave the reactor riser in the different separation means is hereby reduced so as to avoid non-controlled cracking also referred to as after cracking. In order to have an outlet means for the stripping gases in the stripping vessel an opening is present in the conduit between the rough cut cyclone and the secondary cyclone. Preferably this opening is effected by a slit.

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In Figure 1 a separator apparatus according the invention is shown having a hollow circular housing (1), symmetrical around an axis (Ax), fluidly connected to a dipleg (8) a gas outlet tube (4), inlet means (3) for the gas-solids feed, tangentially arranged to create, in use, a vortex flow in the circular housing (1). The inlet means (3) is fluidly connected to an inlet conduit (2). The circular housing (1) has upper tubular portion (5) with a diameter (D3), a frusto-conical envelope as a middle portion (6) of which smallest diameter (D2) is at the lower end and a lower part (7) having a diameter (D1). A tubular sieve (9) with circular openings (10) covers the inlet of the dipleg (8). Also shown is a vortex stabiliser (11) positioned on a hat (12).

In Figure 2 the numbers have the same meaning as in Figure 1. The embodiment disclosed in Figure 2 differs from the one disclosed in Figure 1 in that no widened lower part of the housing is present.

In Figure 3 a tubular sieve (9) is shown with rectangular openings (10) covering the inlet of the dipleg (8) placed in the lower part (7) of the housing. On top of the sieve a vortex stabiliser (11) is positioned. The hat (12) of the vortex stabiliser forms the top of the tubular sieve (9).

Figure 4 represents a preferred stripping vessel (16) of a FCC process having a secondary cyclone according the invention. The upper part of the stripping vessel is shown in which a reactor riser (17) is fluidly connected to a rough cut cyclone (18), which rough cut cyclone is fluidly connected with a gas outlet conduit (19). In the horizontal part of this conduit (19) a slit (21) is present. Conduit (23) is in fluid connection with the tangentially arranged inlet of the secondary cyclone (24). The secondary cyclone (24) has a tubular sieve (25) covering the inlet of the dipleg (26). The

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gaseous product poor in catalyst particles leave the secondary cyclone and the stripping vessel via conduit (27). The lower part of the stripping vessel comprises a fluid bed of catalyst particles (28) to which stripping gas is supplied to via inlet means (29). The dipleg (26) of the secondary cyclone ends about at the upper level of the fluidized bed (28) and the dipleg of the rough cut cyclone (30) ends within the fluidized bed (28). Through the slit (21) stripping gases can enter the inlet of conduit (23) and leave via the secondary cyclone (24) the stripping vessel (16).

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## CLAIMS

1. A separator apparatus for separating solids from a gas-solid containing feed resulting in a gas-rich stream, the separator comprising:

an upright hollow circular housing fluidly connected to a dipleg for discharging solids positioned below the housing;

a gas outlet tube for discharging the gas-rich stream from the circular housing, which outlet tube protrudes substantially co-axial from the top of the housing;

inlet means for the gas-solids feed so arranged to create, in use, a vortex flow in the circular housing;

and a sieve positioned between the lower part of the circular housing and the upper part of the dipleg, which sieve has openings which do not allow particles having a diameter greater than 0.75 times the diameter of the dipleg to pass the sieve and enter the dipleg and wherein the total area of the openings in the sieve is greater than 2 times the cross sectional area of the dipleg.

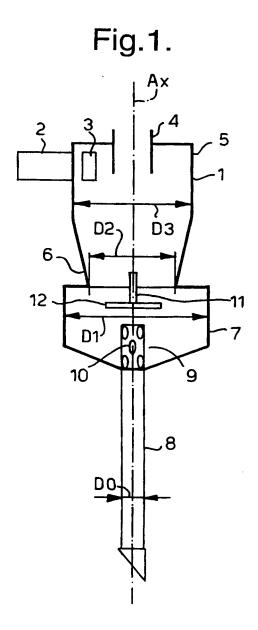
- 2. Apparatus according to claim 1, wherein the openings of the sieve do not allow particles greater than0.5 times the diameter of the dipleg to pass the sieve.
- 3. Apparatus according to any one of claims 1-2, wherein the total area of the openings of the sieve is greater than 5 times the cross sectional area of the dipleg.
- 4. Apparatus according to any one of claims 1-3, wherein a vortex stabiliser is positioned co-axial to the central axis below the opening of the gas outlet and above the sieve.
  - 5. Apparatus according to claim 4, wherein the vortex stabiliser is placed on top of the sieve.

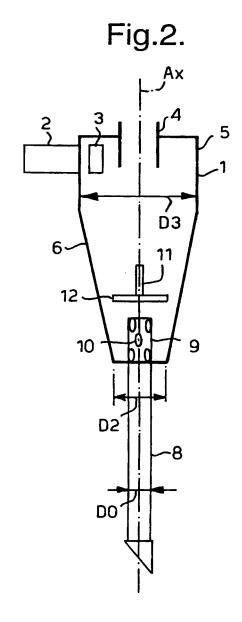
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6. Apparatus according to any one of claims 1-5, wherein the inlet means for the gas-solids feed are tangentially arranged at the upper part of the circular housing.

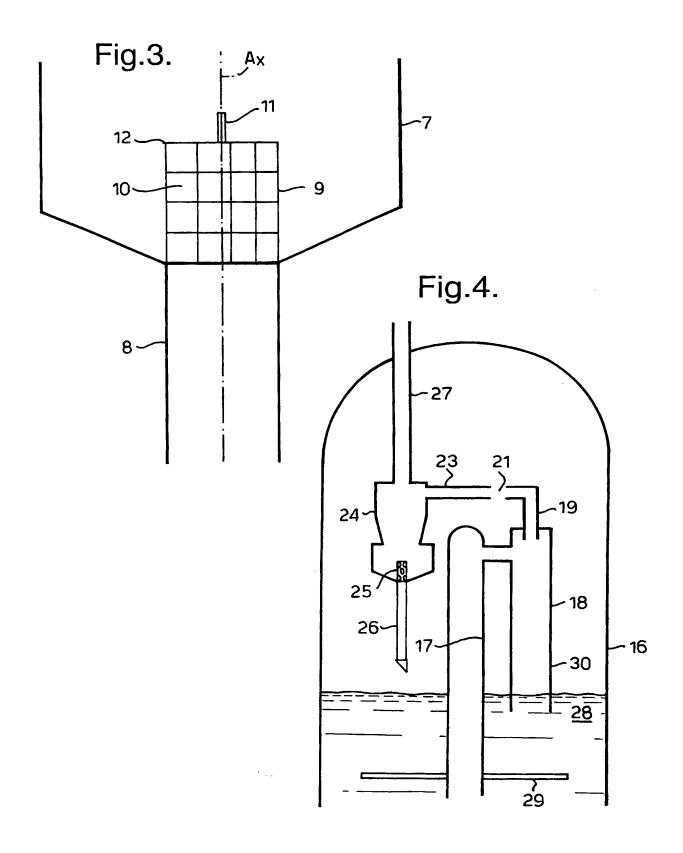
- 7. Apparatus according to any one of claims 1-6, wherein the sieve is a tube placed on top of the dipleg which tube protrudes the circular housing from below, has about the diameter of the dipleg, has an open lower end and a closed upper end and holes are present in the vertical walls of the tube.
- 8. Fluid catalyst cracking process in which catalyst particles are separated from a gaseous reactor effluent in at least two sequential separation steps, wherein the apparatus according to any one of claims 1-7 is used in the second step.

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